

PCT

REQUEST

The undersigned requests that the present international application be processed according to the Patent Cooperation Treaty.

For receiving Office use only	
PCT / CA	00 / 01354
International Application No.	
15 NOVEMBER 2000	(15.11.00)
International Filing Date	
RO/CA	
Name of receiving Office and "PCT International Application"	
Applicant's or agent's file reference (if desired) (12 characters maximum) 4320-207	

Box No. I TITLE OF INVENTION	
IMMERSED MEMBRANE FILTRATION SYSTEM AND OVERFLOW PROCESS	
Box No. II APPLICANT	
Name and address: (Family name followed by given name; for a legal entity, full official designation. The address must include postal code and name of country. The country of the address indicated in this Box is the applicant's State (that is, country) of residence if no State of residence is indicated below.) ZENON ENVIRONMENTAL INC. 3239 Dundas Street West Oakville, Ontario L6N 4B2 Canada	<input type="checkbox"/> This person is also inventor. Telephone No. 905-465-3030 Facsimile No. 905-465-3050 Teleprinter No.
State (that is, country) of nationality: CA	State (that is, country) of residence: CA
This person is applicant for the purposes of: <input type="checkbox"/> all designated States <input checked="" type="checkbox"/> all designated States except the United States of America <input type="checkbox"/> the United States of America only <input type="checkbox"/> the States indicated in the Supplemental Box	
Box No. III FURTHER APPLICANT(S) AND/OR (FURTHER) INVENTOR(S)	
Name and address: (Family name followed by given name; for a legal entity, full official designation. The address must include postal code and name of country. The country of the address indicated in this Box is the applicant's State (that is, country) of residence if no State of residence is indicated below.) JANSON, Arnold 343 Rankin Drive Burlington, Ontario L7N 2B2 Canada	This person is: <input type="checkbox"/> applicant only <input checked="" type="checkbox"/> applicant and inventor <input type="checkbox"/> inventor only (If this check-box is marked, do not fill in below.)
State (that is, country) of nationality: CA	State (that is, country) of residence: CA
This person is applicant for the purposes of: <input type="checkbox"/> all designated States <input type="checkbox"/> all designated States except the United States of America <input checked="" type="checkbox"/> the United States of America only <input type="checkbox"/> the States indicated in the Supplemental Box	
<input checked="" type="checkbox"/> Further applicants and/or (further) inventors are indicated on a continuation sheet.	
Box No. IV AGENT OR COMMON REPRESENTATIVE; OR ADDRESS FOR CORRESPONDENCE	
The person identified below is hereby/has been appointed to act on behalf of the applicant(s) before the competent International Authorities as: <input checked="" type="checkbox"/> agent <input type="checkbox"/> common representative	
Name and address: (Family name followed by given name; for a legal entity, full official designation. The address must include postal code and name of country.) Bereskin & Parr 40 King Street West 40th Floor Toronto, Ontario, Canada M5H 3Y2	Telephone No. (416) 364-7311 Facsimile No. (416) 361-1398 Teleprinter No.
<input type="checkbox"/> Address for correspondence: Mark this check-box where no agent or common representative is/has been appointed and the space above is used instead to indicate a special address to which correspondence should be sent.	



Continuation of Box No. III FURTHER APPLICANT(S) AND/OR (FURTHER) INVENTOR(S)

If none of the following sub-boxes is used, this sheet should not be included in the request.

Name and address: (Family name followed by given name; for a legal entity, full official designation. The address must include postal code and name of country. The country of the address indicated in this Box is the applicant's State (that is, country) of residence if no State of residence is indicated below.)

ADAMS, Nicholas
37 Kipling Road
Hamilton, Ontario
L8S 3X2 Canada

This person is:

- ☐ applicant only
☒ applicant and inventor
☐ inventor only (If this check-box is marked, do not fill in below.)

State (that is, country) of nationality:

CA

State (that is, country) of residence:

CA

This person is applicant for the purposes of:

☐ all designated States

☐ all designated States except the United States of America

☒ the United States of America only

☐ the States indicated in the Supplemental Box

Name and address: (Family name followed by given name; for a legal entity, full official designation. The address must include postal code and name of country. The country of the address indicated in this Box is the applicant's State (that is, country) of residence if no State of residence is indicated below.)

CADERA, Jason
25 Camm Crescent
Guelph, Ontario
N1L 1K2 Canada

This person is:

- ☐ applicant only
☒ applicant and inventor
☐ inventor only (If this check-box is marked, do not fill in below.)

State (that is, country) of nationality:

CA

State (that is, country) of residence:

CA

This person is applicant for the purposes of:

☐ all designated States

☐ all designated States except the United States of America

☒ the United States of America only

☐ the States indicated in the Supplemental Box

Name and address: (Family name followed by given name; for a legal entity, full official designation. The address must include postal code and name of country. The country of the address indicated in this Box is the applicant's State (that is, country) of residence if no State of residence is indicated below.)

COTE, Pierre
26 Tally-Ho Drive
Dundas, Ontario
L9H 3M6 Canada

This person is:

- ☐ applicant only
☒ applicant and inventor
☐ inventor only (If this check-box is marked, do not fill in below.)

State (that is, country) of nationality:

CA

State (that is, country) of residence:

CA

This person is applicant for the purposes of:

☐ all designated States

☐ all designated States except the United States of America

☒ the United States of America only

☐ the States indicated in the Supplemental Box

Name and address: (Family name followed by given name; for a legal entity, full official designation. The address must include postal code and name of country. The country of the address indicated in this Box is the applicant's State (that is, country) of residence if no State of residence is indicated below.)

PEDERSEN, Steven Kristian
498 Rothesay Place
Burlington, Ontario
L7N 3E2 Canada

This person is:

- ☐ applicant only
☒ applicant and inventor
☐ inventor only (If this check-box is marked, do not fill in below.)

State (that is, country) of nationality:

CA

State (that is, country) of residence:

CA

This person is applicant for the purposes of:

☐ all designated States

☐ all designated States except the United States of America

☒ the United States of America only

☐ the States indicated in the Supplemental Box

☐ Further applicants and/or (further) inventors are indicated on another continuation sheet.



No.V DESIGNATION OF STATES

The following designations are hereby made under Rule 4.9(a) (mark the applicable check-boxes; at least one must be marked):

Regional Patent

- ☒ **AP ARIPO Patent:** GH Ghana, GM Gambia, KE Kenya, LS Lesotho, MW Malawi, MZ Mozambique, SD Sudan, SL Sierra Leone, SZ Swaziland, TZ United Republic of Tanzania, UG Uganda, ZW Zimbabwe, and any other State which is a Contracting State of the Harare Protocol and of the PCT
- ☒ **EA Eurasian Patent:** AM Armenia, AZ Azerbaijan, BY Belarus, KG Kyrgyzstan, KZ Kazakhstan, MD Republic of Moldova, RU Russian Federation, TJ Tajikistan, TM Turkmenistan, and any other State which is a Contracting State of the Eurasian Patent Convention and of the PCT
- ☒ **EP European Patent:** AT Austria, BE Belgium, CH and LI Switzerland and Liechtenstein, CY Cyprus, DE Germany, DK Denmark, ES Spain, FI Finland, FR France, GB United Kingdom, GR Greece, IE Ireland, IT Italy, LU Luxembourg, MC Monaco, NL Netherlands, PT Portugal, SE Sweden, and any other State which is a Contracting State of the European Patent Convention and of the PCT
- ☒ **OA OAPI Patent:** BF Burkina Faso, BJ Benin, CF Central African Republic, CG Congo, CI Côte d'Ivoire, CM Cameroon, GA Gabon, GN Guinea, GW Guinea-Bissau, ML Mali, MR Mauritania, NE Niger, SN Senegal, TD Chad, TG Togo, and any other State which is a member State of OAPI and a Contracting State of the PCT (if other kind of protection or treatment desired, specify on dotted line)

National Patent (if other kind of protection or treatment desired, specify on dotted line):

- | | |
|------------------------------------------------------------------------------|----------------------------------------------------------------------------------|
| <input checked="" type="checkbox"/> AE United Arab Emirates | <input checked="" type="checkbox"/> LC Saint Lucia |
| <input checked="" type="checkbox"/> AG Antigua and Barbuda | <input checked="" type="checkbox"/> LK Sri Lanka |
| <input checked="" type="checkbox"/> AL Albania | <input checked="" type="checkbox"/> LR Liberia |
| <input checked="" type="checkbox"/> AM Armenia | <input checked="" type="checkbox"/> LS Lesotho |
| <input checked="" type="checkbox"/> AT Austria | <input checked="" type="checkbox"/> LT Lithuania |
| <input checked="" type="checkbox"/> AU Australia | <input checked="" type="checkbox"/> LU Luxembourg |
| <input checked="" type="checkbox"/> AZ Azerbaijan | <input checked="" type="checkbox"/> LV Latvia |
| <input checked="" type="checkbox"/> BA Bosnia and Herzegovina | <input checked="" type="checkbox"/> MA Morocco |
| <input checked="" type="checkbox"/> BB Barbados | <input checked="" type="checkbox"/> MD Republic of Moldova |
| <input checked="" type="checkbox"/> BG Bulgaria | <input checked="" type="checkbox"/> MG Madagascar |
| <input checked="" type="checkbox"/> BR Brazil | <input checked="" type="checkbox"/> MK The former Yugoslav Republic of Macedonia |
| <input checked="" type="checkbox"/> BY Belarus | <input checked="" type="checkbox"/> MN Mongolia |
| <input checked="" type="checkbox"/> BZ Belize | <input checked="" type="checkbox"/> MW Malawi |
| <input checked="" type="checkbox"/> CA Canada | <input checked="" type="checkbox"/> MX Mexico |
| <input checked="" type="checkbox"/> CH and LI Switzerland and Liechtenstein | <input checked="" type="checkbox"/> MZ Mozambique |
| <input checked="" type="checkbox"/> CN China | <input checked="" type="checkbox"/> NO Norway |
| <input checked="" type="checkbox"/> CR Costa Rica | <input checked="" type="checkbox"/> NZ New Zealand |
| <input checked="" type="checkbox"/> CU Cuba | <input checked="" type="checkbox"/> PL Poland |
| <input checked="" type="checkbox"/> CZ Czech Republic | <input checked="" type="checkbox"/> PT Portugal |
| <input checked="" type="checkbox"/> DE Germany | <input checked="" type="checkbox"/> RO Romania |
| <input checked="" type="checkbox"/> DK Denmark | <input checked="" type="checkbox"/> RU Russian Federation |
| <input checked="" type="checkbox"/> DM Dominica | <input checked="" type="checkbox"/> SD Sudan |
| <input checked="" type="checkbox"/> DZ Algeria | <input checked="" type="checkbox"/> SE Sweden |
| <input checked="" type="checkbox"/> EE Estonia | <input checked="" type="checkbox"/> SG Singapore |
| <input checked="" type="checkbox"/> ES Spain | <input checked="" type="checkbox"/> SI Slovenia |
| <input checked="" type="checkbox"/> FI Finland | <input checked="" type="checkbox"/> SK Slovakia |
| <input checked="" type="checkbox"/> GB United Kingdom | <input checked="" type="checkbox"/> SL Sierra Leone |
| <input checked="" type="checkbox"/> GD Grenada | <input checked="" type="checkbox"/> TJ Tajikistan |
| <input checked="" type="checkbox"/> GE Georgia | <input checked="" type="checkbox"/> TM Turkmenistan |
| <input checked="" type="checkbox"/> GH Ghana | <input checked="" type="checkbox"/> TR Turkey |
| <input checked="" type="checkbox"/> GM Gambia | <input checked="" type="checkbox"/> TT Trinidad and Tobago |
| <input checked="" type="checkbox"/> HR Croatia | <input checked="" type="checkbox"/> TZ United Republic of Tanzania |
| <input checked="" type="checkbox"/> HU Hungary | <input checked="" type="checkbox"/> UA Ukraine |
| <input checked="" type="checkbox"/> ID Indonesia | <input checked="" type="checkbox"/> UG Uganda |
| <input checked="" type="checkbox"/> IL Israel | <input checked="" type="checkbox"/> US United States of America |
| <input checked="" type="checkbox"/> IN India | <input checked="" type="checkbox"/> UZ Uzbekistan |
| <input checked="" type="checkbox"/> IS Iceland | <input checked="" type="checkbox"/> VN Viet Nam |
| <input checked="" type="checkbox"/> JP Japan | <input checked="" type="checkbox"/> YU Yugoslavia |
| <input checked="" type="checkbox"/> KE Kenya | <input checked="" type="checkbox"/> ZA South Africa |
| <input checked="" type="checkbox"/> KG Kyrgyzstan | <input checked="" type="checkbox"/> ZW Zimbabwe |
| <input checked="" type="checkbox"/> KP Democratic People's Republic of Korea | |
| <input checked="" type="checkbox"/> KR Republic of Korea | |
| <input checked="" type="checkbox"/> KZ Kazakhstan | |

Check-box reserved for designating States which have become party to the PCT after issuance of this sheet:



Precautionary Designation Statement: In addition to the designations made above, the applicant also makes under Rule 4.9(b) all other designations which would be permitted under the PCT except any designation(s) indicated in the Supplemental Box as being excluded from the scope of this statement. The applicant declares that those additional designations are subject to confirmation and that any designation which is not confirmed before the expiration of 15 months from the priority date is to be regarded as withdrawn by the applicant at the expiration of that time limit. (Confirmation (including fees) must reach the receiving Office within the 15-month time limit.)



Supplemental Box*If the Supplemental Box is not used, this sheet should not be included in the request.*

1. If, in any of the Boxes, the space is insufficient to furnish all the information: in such case, write "Continuation of Box No. ..." [indicate the number of the Box] and furnish the information in the same manner as required according to the captions of the Box in which the space was insufficient, in particular:

- (i) if more than two persons are involved as applicants and/or inventors and no "continuation sheet" is available: in such case, write "Continuation of Box No. III" and indicate for each additional person the same type of information as required in Box No. III. The country of the address indicated in this Box is the applicant's State (that is, country) of residence if no State of residence is indicated below;
- (ii) if, in Box No. II or in any of the sub-boxes of Box No. III, the indication "the States indicated in the Supplemental Box" is checked: in such case, write "Continuation of Box No. II" or "Continuation of Box No. III" or "Continuation of Boxes No. II and No. III" (as the case may be), indicate the name of the applicant(s) involved and, next to (each) such name, the State(s) (and/or, where applicable, ARIPO, Eurasian, European or OAPI patent) for the purposes of which the named person is applicant;
- (iii) if, in Box No. II or in any of the sub-boxes of Box No. III, the inventor or the inventor/applicant is not inventor for the purposes of all designated States or for the purposes of the United States of America: in such case, write "Continuation of Box No. II" or "Continuation of Box No. III" or "Continuation of Boxes No. II and No. III" (as the case may be), indicate the name of the inventor(s) and, next to (each) such name, the State(s) (and/or, where applicable, ARIPO, Eurasian, European or OAPI patent) for the purposes of which the named person is inventor;
- (iv) if, in addition to the agent(s) indicated in Box No. IV, there are further agents: in such case, write "Continuation of Box No. IV" and indicate for each further agent the same type of information as required in Box No. IV;
- (v) if, in Box No. V, the name of any State (or OAPI) is accompanied by the indication "patent of addition," or "certificate of addition," or if, in Box No. V, the name of the United States of America is accompanied by an indication "continuation" or "continuation-in-part": in such case, write "Continuation of Box No. V" and the name of each State involved (or OAPI), and after the name of each such State (or OAPI), the number of the parent title or parent application and the date of grant of the parent title or filing of the parent application;
- (vi) if, in Box No. VI, there are more than three earlier applications whose priority is claimed: in such case, write "Continuation of Box No. VI" and indicate for each additional earlier application the same type of information as required in Box No. VI;
- (vii) if, in Box No. VI, the earlier application is an ARIPO application: in such case, write "Continuation of Box No. VI", specify the number of the item corresponding to that earlier application and indicate at least one country party to the Paris Convention for the Protection of Industrial Property or one Member of the World Trade Organization for which that earlier application was filed.

2. If, with regard to the precautionary designation statement contained in Box No. V, the applicant wishes to exclude any State(s) from the scope of that statement: in such case, write "Designation(s) excluded from precautionary designation statement" and indicate the name or two-letter code of each State so excluded.

3. If the applicant claims, in respect of any designated Office, the benefits of provisions of the national law concerning non-prejudicial disclosures or exceptions to lack of novelty: in such case, write "Statement concerning non-prejudicial disclosures or exceptions to lack of novelty" and furnish that statement below.

Continuation of Box No. VI:

CA: 2,308,230; 05 May 2000 (05. 05. 00)

US: 09/565,032; 05 May 2000 (05. 05. 00)



2

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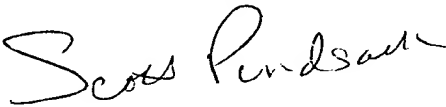
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Box No. VI PRIORITY CLAIM		<input checked="" type="checkbox"/> Further priority claims are indicated in the Supplemental Box.		
Filing date of earlier application (day/month/year)	Number of earlier application	Where earlier application is:		
		national application: country	regional application:* regional Office	international application: receiving Office
item (1) 18 November 1999	2,290,053	CA		
item (2) 18 November 1999	PCT/CA99/01113			CA
item (3) 17 February 2000	09/505,718	US		
<input type="checkbox"/> The receiving Office is requested to prepare and transmit to the International Bureau a certified copy of the earlier application(s) (only if the earlier application was filed with the Office which for the purposes of the present international application is the receiving Office) identified above as item(s): (1) (2) (4) -				
* Where the earlier application is an ARIPO application, it is mandatory to indicate in the Supplemental Box at least one country party to the Paris Convention for the Protection of Industrial Property for which that earlier application was filed (Rule 4.10(b)(ii)). See Supplemental Box.				
Box No. VII INTERNATIONAL SEARCHING AUTHORITY				
Choice of International Searching Authority (ISA) (if two or more International Searching Authorities are competent to carry out the international search, indicate the Authority chosen; the two-letter code may be used):		Request to use results of earlier search; reference to that search (if an earlier search has been carried out by or requested from the International Searching Authority): Date (day/month/year) Number Country (or regional Office)		
ISA / EPO				
Box No. VIII CHECK LIST; LANGUAGE OF FILING				
This international application contains the following number of sheets: request : 5 description (excluding sequence listing part) : 9 claims : 4 abstract : 1 drawings : 3 sequence listing part of description : Total number of sheets : 22		This international application is accompanied by the item(s) marked below: 1. <input checked="" type="checkbox"/> fee calculation sheet 2. <input type="checkbox"/> separate signed power of attorney 3. <input type="checkbox"/> copy of general power of attorney; reference number, if any: 4. <input type="checkbox"/> statement explaining lack of signature 5. <input type="checkbox"/> priority document(s) identified in Box No. VI as item(s): 6. <input type="checkbox"/> translation of international application into (language): 7. <input type="checkbox"/> separate indications concerning deposited microorganism or other biological material 8. <input type="checkbox"/> nucleotide and/or amino acid sequence listing in computer readable form 9. <input type="checkbox"/> other (specify):		
Figure of the drawings which should accompany the abstract:		Language of filing of the international application: English		
Box No. IX SIGNATURE OF APPLICANT OR AGENT				
Next to each signature, indicate the name of the person signing and the capacity in which the person signs (if such capacity is not obvious from reading the request).				
SCOTT PUNDSACK  Bereskin & Parr Agents for the Applicant				

For receiving Office use only		2. Drawings: <input checked="" type="checkbox"/> received: <input type="checkbox"/> not received:
1. Date of actual receipt of the purported international application:	15 NOVEMBER 2000 (15 11 00)	
3. Corrected date of actual receipt due to later but timely received papers or drawings completing the purported international application:		
4. Date of timely receipt of the required corrections under PCT Article 11(2):		
5. International Searching Authority (if two or more are competent): ISA /	6. <input type="checkbox"/> Transmittal of search copy delayed until search fee is paid.	

For International Bureau use only
Date of receipt of the record copy by the International Bureau:



PCT

FEE CALCULATION SHEET Annex to the Request

For receiving Office use only

PCT / CA 00 / 01354
International application No.

15 NOVEMBER 2000 15.11.00
Date stamp of the receiving Office

Applicant's or agent's
file reference

4320-207

Applicant

ZENON ENVIRONMENTAL INC. ET AL

CALCULATION OF PRESCRIBED FEES

1. TRANSMITTAL FEE

\$200.00 T

2. SEARCH FEE

\$1,249.00 S

International search to be carried out by

(If two or more International Searching Authorities are competent in relation to the international application, indicate the name of the Authority which is chosen to carry out the international search.)

3. INTERNATIONAL FEE

Basic Fee

The international application contains 22 sheets.

first 30 sheets

\$562.00 b1

0

x

\$13.00

=

\$0.00 b2

remaining sheets

additional amount

\$562.00 B

Add amounts entered at b1 and b2 and enter total at B

Designation Fees

The international application contains 87 designations.

8

x

\$121.00

=

\$968.00 D

number of designation fees
payable (maximum 8)

amount of designation fee

Add amounts entered at B and D and enter total at I

\$1,530.00 I

(Applicants from certain States are entitled to a reduction of 75% of the international fee. Where the applicant is (or all applicants are) so entitled, the total to be entered at I is 25% of the sum of the amounts entered at B and D.)

4. FEE FOR PRIORITY DOCUMENT (if applicable)

P

5. TOTAL FEES PAYABLE

\$2,979.00

Add amounts entered at T, S, I and P, and enter total in the TOTAL box

TOTAL

☐ The designation fees are not paid at this time.

MODE OF PAYMENT

☐ authorization to charge
deposit account (see below)

☐ bank draft

☐ coupons

☐ cheque

☐ cash

☒ other (specify): VISA

☐ postal money order

☐ revenue stamps

DEPOSIT ACCOUNT AUTHORIZATION (this mode of payment may not be available at all receiving Offices)

The RO/ ☐ is hereby authorized to charge the total fees indicated above to my deposit account.

☐ (this check-box may be marked only if the conditions for deposit accounts of the receiving Office so permit) is hereby authorized to charge any deficiency or credit any overpayment in the total fees indicated above to my deposit account.

☐ is hereby authorized to charge the fee for preparation and transmittal of the priority document to the International Bureau of WIPO to my deposit account.

Deposit Account No.

Date (day/month/year)

Signature



INTERNATIONAL SEARCH REPORT

(PCT Article 18 and Rules 43 and 44)

Applicant's or agent's file reference 4320-207	FOR FURTHER ACTION see Notification of Transmittal of International Search Report (Form PCT/ISA/220) as well as, where applicable, item 5 below.	
International application No. PCT/CA 00/ 01354	International filing date (day/month/year) 15/11/2000	(Earliest) Priority Date (day/month/year) 18/11/1999
Applicant ZENON ENVIRONMENTAL INC. et al.		

This International Search Report has been prepared by this International Searching Authority and is transmitted to the applicant according to Article 18. A copy is being transmitted to the International Bureau.

This International Search Report consists of a total of 3 sheets.

☒ It is also accompanied by a copy of each prior art document cited in this report.

1. Basis of the report

- a. With regard to the **language**, the international search was carried out on the basis of the international application in the language in which it was filed, unless otherwise indicated under this item.

☐ the international search was carried out on the basis of a translation of the international application furnished to this Authority (Rule 23.1(b)).

- b. With regard to any **nucleotide and/or amino acid sequence** disclosed in the international application, the international search was carried out on the basis of the sequence listing :

☐ contained in the international application in written form.

☐ filed together with the international application in computer readable form.

☐ furnished subsequently to this Authority in written form.

☐ furnished subsequently to this Authority in computer readable form.

☐ the statement that the subsequently furnished written sequence listing does not go beyond the disclosure in the international application as filed has been furnished.

☐ the statement that the information recorded in computer readable form is identical to the written sequence listing has been furnished

2. ☐ **Certain claims were found unsearchable** (See Box I).

3. ☐ **Unity of invention is lacking** (see Box II).

4. With regard to the **title**,

☒ the text is approved as submitted by the applicant.

☐ the text has been established by this Authority to read as follows:

5. With regard to the **abstract**,

☒ the text is approved as submitted by the applicant.

☐ the text has been established, according to Rule 38.2(b), by this Authority as it appears in Box III. The applicant may, within one month from the date of mailing of this international search report, submit comments to this Authority.

6. The figure of the **drawings** to be published with the abstract is Figure No.

☐ as suggested by the applicant.

☒ because the applicant failed to suggest a figure.

☐ because this figure better characterizes the invention.

2
☐ None of the figures.



100

INTERNATIONAL SEARCH REPORT

International Application No

PCT/CA 00/01354

A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 B01D65/02 B01D65/06 B01D63/02 B01D63/04 C02F3/06

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 B01D C02F

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

WPI Data, PAJ, EPO-Internal

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	PATENT ABSTRACTS OF JAPAN vol. 1997, no. 02, 28 February 1997 (1997-02-28) & JP 08 281082 A (KUBOTA CORP), 29 October 1996 (1996-10-29) abstract	1, 8, 19
A	--- PATENT ABSTRACTS OF JAPAN vol. 1999, no. 04, 30 April 1999 (1999-04-30) & JP 11 000534 A (KURITA WATER IND LTD), 6 January 1999 (1999-01-06) abstract	10-18
A	--- DE 296 20 426 U (PREUSSAG NOELL WASSESTECHNIK) 30 April 1997 (1997-04-30) claims; figures --- -/--	10-18

☒ Further documents are listed in the continuation of box C.☒ Patent family members are listed in annex.

* Special categories of cited documents :

- *A* document defining the general state of the art which is not considered to be of particular relevance
- *E* earlier document but published on or after the international filing date
- *L* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- *O* document referring to an oral disclosure, use, exhibition or other means
- *P* document published prior to the international filing date but later than the priority date claimed

- *T* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
- *X* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
- *Y* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.
- *&* document member of the same patent family

Date of the actual completion of the international search

2 March 2001

Date of mailing of the international search report

10/04/2001

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl,
Fax: (+31-70) 340-3016

Authorized officer

Cordero Alvarez, M

INTERNATIONAL SEARCH REPORT

International Application No

PCT/CA 00/01354

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	PATENT ABSTRACTS OF JAPAN vol. 1997, no. 06, 30 June 1997 (1997-06-30) & JP 09 047762 A (TOTO LTD), 18 February 1997 (1997-02-18) abstract ---	1,6,7,9, 15,16,20
A	PATENT ABSTRACTS OF JAPAN vol. 1997, no. 12, 25 December 1997 (1997-12-25) & JP 09 220569 A (KUBOTA CORP), 26 August 1997 (1997-08-26) abstract -----	1

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/CA 00/01354

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
JP 08281082	A	29-10-1996	NONE	
JP 11000534	A	06-01-1999	NONE	
DE 29620426	U	20-03-1997	NONE	
JP 09047762	A	18-02-1997	NONE	
JP 09220569	A	26-08-1997	NONE	



Patent Abstracts of Japan

PUBLICATION NUMBER : 08281082
PUBLICATION DATE : 29-10-96

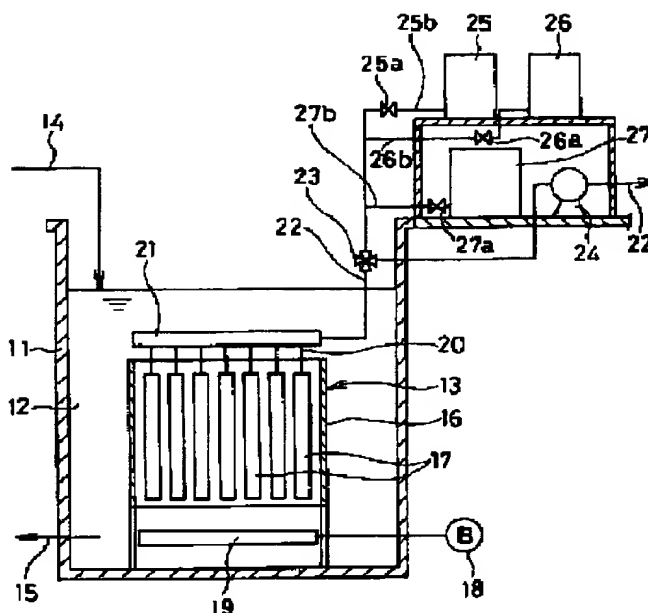
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APPLICANT : KUBOTA CORP;

INVENTOR : NURISHI MASA HARU;

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TITLE : WASHING METHOD OF IMMERSION
TYPE MEMBRANE CARTRIDGE



ABSTRACT : PURPOSE: To efficiently and economically wash an immersion type membrane cartridge without taking it out from a treating tank.

CONSTITUTION: In the state that the immersion type membrane cartridge is immersed into an activated sludge mixture liquid 12 and filtering and aeration are stopped, a chemical liquid is poured into a permeated water flow path of the membrane cartridge 17 under low pressure to be held for a proper time, and next clean water is poured into the permeated water flow path while the chemical liquid is permeated to a liquid side to be treated, to replace the inside of the permeated water flow path with the clean water.

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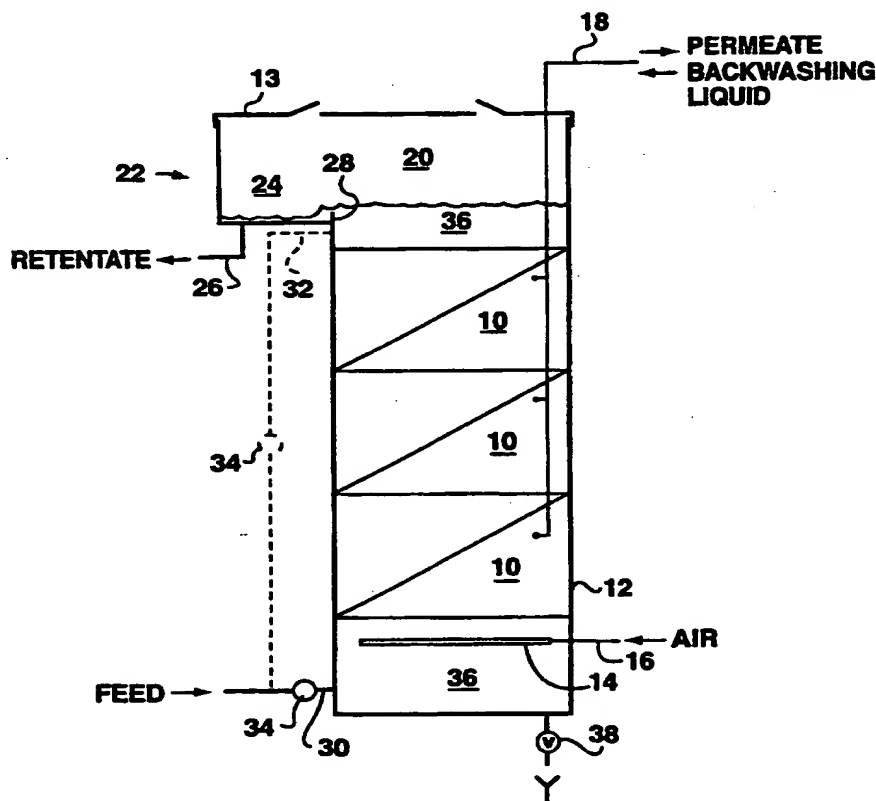
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(54) Title: **IMMERSED MEMBRANE FILTRATION SYSTEM AND OVERFLOW PROCESS**



(57) Abstract: Modules of ultrafiltration or microfiltration membranes are arranged in a tank open to the atmosphere to substantially cover the cross sectional area of the tank. A filtration cycle has permeation steps and deconcentration steps. During permeation, supply of feed substantially equals feed removed and little if any aeration is used. During deconcentration, aeration with scouring bubbles is provided with one or both of backwashing and feed flushing. In feed flushing, feed water is supplied to the tank from below the modules. Excess tank water created during deconcentration flows generally upwards through the modules and out through a retentate outlet or overflow at the top of the tank.

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Title: Immersed Membrane Filtration System and Overflow Process**FIELD OF THE INVENTION**

5 This invention relates to a filtration system using immersed suction driven filtering membranes to filter water, for example, to filter surface water to produce potable water, and to a method of operating such a system.

BACKGROUND OF THE INVENTION

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 A prior art immersed membrane water filtration system is shown in Figure 1. An open tank (a) holds a membrane module (b) immersed in tank water (c). Feed water to be filtered flows into the tank, typically continuously. Suction on an inner surface of the membranes in the
15 membrane module (b) draws filtered permeate through the membrane wall. Solids are rejected by the membranes and accumulate in the tank water (c). Solids rich retentate is continuously or periodically drained from the tank.

20 The membrane module (b) is cleaned in part by backwashing and aeration. In backwashing, a backwashing liquid (typically permeate or permeate with a chemical additive) is pumped into the inner spaces of the membranes and flows into the tank water (c). In aeration, air bubbles are
25 created at an aerator (d) mounted below the membrane module (c). The air bubbles agitate and scour the membranes and create an air lift effect. The air lift effect moves tank water (c) in a recirculation pattern (e) upwards through the membrane module (b) and in a downcomer (f) through spaces between the perimeter of the module (b) and the sides of the tank (a). The
30 tank water (c) flowing in the recirculation pattern (e) further physically cleans the membranes and disperses solids rich water from near the membrane module (b).

SUMMARY OF THE INVENTION

It is an object of the present invention to improve on the prior art. This object is met by the combination of features, steps or both found in the independent claims, the dependent claims disclosing further advantageous
5 embodiments of the invention. The following summary may not describe all necessary features of the invention which may reside in a sub-combination of the following features or in a combination with features described in other parts of this document.

10

In various aspects of the invention, a filtration system having immersed suction driven filtering membranes is used to filter water containing low concentrations of suspended solids, for example, to filter surface water to produce potable water. A process is provided for operating
15 such a system.

Membrane modules are arranged in a tank open to the atmosphere and fill most of its horizontal cross sectional area. An upper portion of the tank encloses a volume directly above the modules. This upper portion of
20 the tank is provided with a retentate outlet from the tank. Tank water that is not withdrawn as permeate flows out of the tank through the retentate outlet.

Permeate is withdrawn by suction on an inner surface of the
25 membranes, preferably at a flux between 10 and 60 L/m²/h, more preferably between 20 and 40 L/m²/h. Feed water is added to the tank at a rate that substantially equals the rate at which permeate is withdrawn. Thus during permeation little if any tank water flows out of the outlet and the level of the tank water remains above the membranes.

30

Permeation is stopped periodically for a deconcentration step. During the deconcentration step the membranes are backwashed, feed flow is

provided from below the modules or both. Tank water rises through the modules, the water level in the tank rises and tank water containing solids (then called retentate) flows out of the retentate outlet to deconcentrate the tank water. Aeration with scouring bubbles is provided during the
5 deconcentration step.

BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 is a schematic representation of a prior art filtration system.

10 Figure 2 is a schematic representation of a filtering reactor made in accordance with a preferred embodiment of the present invention.

Figure 3 is a plan view of a filtering reactor made in accordance with a preferred embodiment of the present invention.

15 DETAILED DESCRIPTION OF EMBODIMENTS

Referring to Figure 2, three membrane modules 10 are stacked on top of each other in a tank 12. The tank 12 is open to the atmosphere although it may be covered with a vented lid 13. The membrane modules 10 may
20 contain flat sheet or hollow fibre membranes with pore sizes in the microfiltration or ultrafiltration range, preferably between 0.003 and 10 microns and more preferably between 0.01 and 1.0 microns. An inner surface of the membranes is connected to one or more headers. An aerator 14 is mounted below the membrane modules 10. The aerator 14 is
25 connected to an air supply pipe 14 in turn connected to a supply of air, nitrogen or other suitable gas. The membrane modules 10 include, within their horizontal cross-sectional area, channels for water and air bubbles to flow vertically through the membrane modules 10 to agitate or scour the membranes. When membrane modules 10 are stacked on top of each other,
30 they are aligned such that water can flow vertically through the stack.

Preferably, the membrane modules 10 contain hollow fibre membranes oriented horizontally and mounted in a slightly slackened state between pairs of horizontally spaced, vertically extending headers. One example is formed of several elements placed side-by-side, each element
5 having a large number of fibres of between 0.2 and 1.0 mm outside diameter and between 0.2 m and 1.0 m in length (the shorter length used for the smaller diameter fibres and the longer length used for larger diameter fibres) potted at either end in a header but with permeate withdrawn from only one header. The elements may be separated by impervious vertical
10 plates. Such modules can provide 500 to 1500 m² of membrane surface area for each m² of horizontal cross-sectional area of a large municipal or commercial tank and there is minimal channeling or dead zones when tank water flows through the modules.

15 The membrane modules 10 are sized and positioned to fill most of the horizontal cross-sectional area of the tank 12 leaving room only for necessary fittings and other apparatus and maintenance or set-up procedures. Space is not provided for downcomers outside the perimeter of the modules 10 and baffles are provided if necessary to block flow through
20 any space left for fittings etc. or otherwise outside the perimeter of the membrane modules 10. Preferably more than 90%, more preferably substantially all, of the horizontal cross-sectional area of the tank 12 is filled with membrane modules 10.

25 A permeate pipe 18 connects the headers of the membrane modules 10 to means for permeating by suction on the inner surfaces of the membranes and backwashing means. Such means are known in the art and allow the permeate pipe 18 to be used to either withdraw permeate from the tank 12 or to flow a backwashing liquid (typically permeate or permeate
30 mixed with a chemical) in a reverse direction through the membranes and into the tank 12 in which the backwashing liquid becomes part of tank water 36.

An upper portion 20 of the tank 12 is provided with a retentate outlet 22 having an overflow area 24 connected to a drain pipe 26 to remove retentate from the tank 12. Retentate outlet 22 preferably incorporates an overflow or weir 28 which helps foam produced by aeration (otherwise a cleanliness, safety or volatile chemical release problem) to flow into the overflow area 24. The retentate outlet 22 preferably also has sufficient capacity to release expected flows of retentate quickly to reduce the required free board of the tank 12.

Feed water enters the tank 12 through a first inlet 30 or a second inlet 32 as determined by feed valves 34. Once in the tank 12, feed water may be called tank water 36 which flows generally upwards or downwards through the membrane modules 10.

A filtration cycle has a permeation step followed by a deconcentration step and is repeated many times between more intensive maintenance or recovery cleaning procedures. The permeation step typically lasts for about 15 to 60 minutes, preferably 20 to 40 minutes and is carried out in the absence of aeration. Permeate flux is preferably between 10 and 60 L/m²/h, more preferably between 20 and 40 L/m²/h, wherein the surface area of hollow fibre membranes is based on the outside diameter of the membranes.

During permeation, feed water is added to the tank 12 from one of the inlets 30, 32 at substantially the rate at which permeate is withdrawn. Tank water 36 flows through the membrane modules 10 to generally replace permeate as it is withdrawn from the tank 12. Thus during permeation little if any tank water 36 flows out of the retentate outlet 22 and the level of the tank water 36 remains above the membranes. If the membrane module 10 acts to some extent like a media filter (as will some membrane modules 10 of tightly packed horizontally oriented hollow fibre membranes), feed

preferably enters the tank 12 through the second inlet 32. In this way, solids in some feed waters are preferentially deposited in the upper membrane module 10, closer to the retentate outlet 22 and where the upward velocity of the tank water 36 during a deconcentration step will be the greatest, as will be explained below. This set-up is also useful in retrofitting sand filters which are typically set up to receive feed from the top and to backwash from below. For other membrane modules 10, installations or feed waters, the first inlet 30 may be used during permeation.

10 The deconcentration step commences when permeation stops and lasts for about 20 to 90 seconds, preferably 30 to 60 seconds. During the deconcentration step, scouring bubbles are produced at the aerator 14 and rise through the membrane modules 10. In addition one or both of the steps of backwashing and feed flushing are performed. To flush with feed
15 water, feed enters the tank 12 through the first inlet 30 creating an excess of tank water 36 which rises upwards through the membrane modules 10. The rate of flow of feed water during feed flushing is typically between 0.5 and 2, preferably between 0.7 and 1.5, times the rate of flow of feed water during permeation. With either backwashing or feed flushing, the level of
20 the tank water 36 rises, tank water 36 flows upwards through the membrane modules 10 and tank water 36 containing solids (then called retentate) flows out of the retentate outlet 22 to deconcentrate the tank water 36.

In some cases, the upwards velocity of the tank water 36 may create
25 forces on the membranes that exceed their strength, particularly if strong feed flushing and back washing are performed simultaneously. In these cases, the rate of flow of feed water or backwash liquid or both can be reduced to reduce the upward velocity of the tank water 36. Alternatively, the flow of feed water can be turned off during backwashing and any feed
30 flushing done while there is no backwashing and vice versa. For example, a deconcentration step may involve backwashing preferably with aeration but without feed flushing for a first part of the deconcentration step and feed

flushing preferably with aeration but without backwashing for a second part of the deconcentration step. Further alternatively, deconcentration steps involving backwashing preferably with aeration but without feed flushing can be performed in some cycles and deconcentration steps involving feed
5 flushing preferably with aeration but without backwashing can be used in other cycles. Other combinations of the above procedures might also be used.

Aeration is typically performed at the same time as the other steps to
10 reduce the total time of the deconcentration step. Aeration may, however, begin several seconds (approximately the time required for a bubble to rise from the aerator 14 to the surface of the tank water 36) before backwashing or feed flushing. Such aeration in the absence of tank water 36 flow (because no space was left for downcomers) causes turbulence which help
15 loosen some foulants and float some solids to near the top of the tank 12 before retentate starts flowing out the retentate outlet 20.

Aeration during the deconcentration step does not need to overcome suction to dislodge solids from the membranes and is provided at a
20 superficial velocity (m^3/h of air at standard conditions per m^2 of module cross-sectional area) between 25 m/h and 75 m/h . For many if not most feed waters, particularly those feed waters having low turbidity and solids concentrations less than about 500 mg/L , additional aeration is not required. Nevertheless, a smaller amount of aeration may be provided with difficult
25 feed water during permeation to disperse solids from dead zones in a membrane module 10 and homogenize the tank water 36. For this purpose, aeration is provided at a superficial velocity less than 25 m/h or intermittently at the higher rates described above.

30 During the deconcentration step, the feed water or backwashing liquid introduced into the tank 12 creates a flow of tank water 36 upwards through the modules 10. The tank water 36 flowing through the membrane

modules 10 helps remove solids loosened by the scouring bubbles from the membrane modules 10 and also directly acts on the surface of the membranes. The tank water 36 flows most rapidly near the top of the tank 12 which helps reduce preferential fouling of upper membranes when membrane modules 10 are stacked, for example to depths of 2 m or more. Some solids in the tank water 36 may have a settling velocity greater than the velocity of the upflow velocity and will settle. The volume of these solids is small and they may be removed from time to time by partially draining the tank 12 through a supplemental drain 38.

10

Based on a design permeate flux, the required flow of feed water during permeation can be calculated and delivered, typically by adjusting a feed pump or feed valve. The frequency and intensity of deconcentration events is then selected to achieve a desired loss in membrane permeability over time. If flux during permeation is kept below about 60 L/m²/h, preferably less than 40 L/m²/h, the inventors have found that surprising little fouling occurs and the periodic deconcentration events are usually sufficient. More surprisingly, the energy cost savings produced by operating at low flux and low aeration more than offsets the cost of filling the tank 12 with membrane modules 10. Despite the low flux (compared to a more typical flux of 50 to 100 L/m²/h), high tank velocities (flux of permeate in m³/h divided by tank horizontal cross sectional area in m²) are achieved which compare favourably with sand filtration. Further, resulting recovery rates are generally adequate for single stage filtration and are typically adequate for the first stage of two stage filtration (wherein the retentate is re-filtered) even with aggressive deconcentration.

Figure 3 shows a plan view of a larger filtering reactor. A second tank 200 encloses several cassettes 220 each of which may contain a plurality of membrane modules. Open channels 202 are provided between adjacent cassettes 220 to receive tank water overflowing the cassettes 210 as described above. The channels 202 are sloped to drain towards a larger trough 204

which is in turn sloped to drain towards a second outlet 206. The second outlet 206 has an outlet box 208 to temporarily hold the discharged tank water before it flows into a drain pipe 210. As in the embodiment of figure 9, feed water enters the second tank 200 at a point below the cassettes 220, 5 but several second inlets 212 are attached to an inlet header 214 to provide a distributed supply of feed.

It is to be understood that what has been described are preferred embodiments of the invention for example and without limitation to the 10 combination of features necessary for carrying the invention into effect. The invention may be susceptible to certain changes and alternative embodiments without departing from the subject invention, the scope of which is defined in the following claims.

We claim:

1. A process of filtering water comprising the steps of,
 - (a) providing one or more modules of filtering membranes immersed in water in a tank open to the atmosphere;
 - (b) providing a retentate outlet from a portion of the tank above the one or more modules;
 - (c) permeating filtered water by (i) adding a selected volume of feed water to the tank and (ii) withdrawing substantially the selected volume of water through the one or more modules as permeate;
 - (d) periodically stopping permeation to perform a deconcentration step, the deconcentration step further comprising providing scouring bubbles from below the modules and at least one of (I) backwashing or (II) providing a flow of feed water into the tank from below the modules or both (I) and (II); and,
 - (e) flowing excess water containing retained solids out of the retentate outlet during the deconcentration step.
2. The process of claim 1 wherein the modules cover most of the horizontal cross sectional area of the tank.
3. The process of claim 1 wherein the modules cover more than 90% of the horizontal cross sectional area of the tank.
4. The process of claim 1 wherein the modules cover substantially all of the horizontal cross sectional area of the tank.
5. The process of claim 1 wherein aeration is commenced before backwashing.

6. The process of claim 1 wherein the filtering membranes are hollow fibres oriented horizontally.
7. The process of claim 4 wherein the filtering membranes are hollow fibres oriented horizontally.
8. A process of filtering water comprising,
repeating a filtration cycle having
 - (a) a permeation step wherein,
 - (i) feed water enters a tank; and,
 - (ii) a similar volume of permeate is withdrawn from the tank by suction on an inner surface of submerged filtering membranes; and,
 - (b) a deconcentration step wherein,
 - (iii) scouring bubbles rise through the modules;
 - (iv) the membranes are backwashed; and,
 - (v) water containing solids flows upwards through the modules and exits the tank.
9. The process of claim 8 wherein the filtering membranes are hollow fibres oriented horizontally.
10. A filtering reactor comprising,
 - (a) a tank open to the atmosphere;
 - (b) one or more modules of suction driven filtering membranes in the tank for withdrawing a filtered permeate;
 - (c) an inlet to add feed water to the tank from below the one or more modules;
 - (d) a retentate outlet to discharge water containing retained solids from the tank from above the one or more modules; and,
 - (e) an aerator below the one or more modules.

11. The reactor of claim 10 wherein the modules cover most of the horizontal cross sectional area of the tank.
12. The reactor of claim 10 wherein the modules cover more than 90% of the horizontal cross sectional area of the tank.
13. The reactor of claim 10 wherein the modules cover substantially all of the horizontal cross sectional area of the tank.
14. The reactor of claim 10 wherein the retentate outlet incorporates an overflow or weir.
15. The reactor of claim 10 wherein the filtering membranes are hollow fibres oriented horizontally.
16. The reactor of claim 13 wherein the filtering membranes are hollow fibres oriented horizontally.
17. The process of claim 8 wherein feed water is provided from above the modules during permeation.
18. The process of claim 9 wherein feed water is provided from above the modules during permeation.
19. A process of filtering water comprising,
repeating a filtration cycle having
 - (a) a permeation step wherein,
 - (i) feed water enters a tank; and,
 - (ii) a similar volume of permeate is withdrawn from the tank by suction on an inner surface of submerged filtering membranes; and,
 - (b) a deconcentration step wherein,
 - (iii) scouring bubbles rise through the modules;

- (iv) feed water flows into the tank from below the modules; and,
- (v) water containing solids flows upwards through the modules and exits the tank.

20. The process of claim 19 wherein the filtering membranes are hollow fibres oriented horizontally.

INTERNATIONAL SEARCH REPORT

International Application No
PCT/CA 00/01354

A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 B01D65/02 B01D65/06 B01D63/02 B01D63/04 C02F3/06

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 B01D C02F

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

WPI Data, PAJ, EPO-Internal

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	PATENT ABSTRACTS OF JAPAN vol. 1997, no. 02, 28 February 1997 (1997-02-28) & JP 08 281082 A (KUBOTA CORP), 29 October 1996 (1996-10-29) abstract	1, 8, 19
A	PATENT ABSTRACTS OF JAPAN vol. 1999, no. 04, 30 April 1999 (1999-04-30) & JP 11 000534 A (KURITA WATER IND LTD), 6 January 1999 (1999-01-06) abstract	10-18
A	DE 296 20 426 U (PREUSSAG NOELL WASSERTECHNIK) 30 April 1997 (1997-04-30) claims; figures	10-18
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☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

* Special categories of cited documents :

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X document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

Y document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

G document member of the same patent family

Date of the actual completion of the international search

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INTERNATIONAL SEARCH REPORT

Intern: 31 Application No

PCT/CA 00/01354

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

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